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# H-sorption in MgH<sub>2</sub> nanocomposites containing Fe or Ni with fluorine

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### Abstract

Ball milling techniques were used to introduce both fluorine and catalytic transition metals (Fe, Ni) into MgH<sub>2</sub> nanograined powders. XRD was carried out to follow the structural evolution upon milling, whereas the thermal stability against H-desorption was investigated by DSC and TG analysis. The latter showed that fluorine additions with the Fe catalyst effectively decrease the desorption temperature to about 500 K. Results on the absorption/desorption kinetics, which was investigated by volumetric techniques, are presented and discussed with respect to both the simultaneous catalytic activity of Fe or Ni with F and the effect of solid-state processes which may occur upon mechanical alloying. © 2005 Elsevier B.V. All rights reserved.

Keywords: Hydrogen storage materials; High-energy ball milling

## 1. Introduction

Magnesium hydride is considered as one of the most attractive candidate materials for hydrogen storage, due to its high capacity (about 7.6 wt.%) and low cost. Yet, it exhibits, even at high temperatures, a slow absorption and desorption kinetics, which, up to now, has severely limited any practical application [1]. Many investigations have, therefore, focused on improving the reaction kinetics by both tailoring the MgH<sub>2</sub> microstructure and adding a proper catalyst. For instance, it has been shown [2] that processing  $MgH_2$  by high-energy ball milling techniques is beneficial, as fresh and clean surfaces are created at each impact and different kind of crystalline defects are introduced in the lattice. At the same time, MgH<sub>2</sub> grains are reduced to nanometer scale, the resulting path for hydrogen bulk diffusion within the material being significantly shortened. Ball milling has been also used for producing nano-composites in which MgH<sub>2</sub> is blended with transition metals (e.g. V, Ti, Fe, and Ni) [3] or transition metal oxides, such as Nb<sub>2</sub>O<sub>5</sub> or V<sub>2</sub>O<sub>5</sub> [4]. In such cases, the metallic or metallic oxide particles are reported to effectively act

as catalysts, fast hydrogen-sorption kinetics being achieved. Improved kinetics has been also reported when Mg-Ni eutectic alloys undergo a fluorination treatment in aqueous solution [5]. For the latter, it is argued that the formation of a fluorinated surface layer enhances hydrogen reactivity and protects the material from passivation.

In this paper, we report on preliminary results for ballmilled MgH<sub>2</sub>-nanocomposites containing FeF<sub>3</sub> or NiF<sub>2</sub>, which were chosen in order to combine the catalytic effect of transition metals with the possible benefits of fluorinated compounds [6].

## 2. Experimental

Ball milling was performed in a Fritsch Pulverizette P0 using hardened steel balls and vials. The starting powders (MgH<sub>2</sub> from Sigma-Aldrich, 90% purity, the rest being magnesium; FeF<sub>3</sub> anhydrous from Alfa Aesar, 97% purity; and NiF<sub>2</sub> anhydrous from Strem Chemicals, 99% purity) were charged in the vials in order to have powder mixtures consisting of either MgH<sub>2</sub> + 5 mol% FeF<sub>3</sub> or MgH<sub>2</sub> + 5 mol% NiF<sub>2</sub>. The total amount of the starting mixture charged in each vial resulted in a ball-to-powder weight ratio, which

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exceeded 20:1. The milling time was in each case 48 h. All the powder handling before and after milling was carried out in a glove box under a protecting argon atmosphere.

Structural characterization was performed by X-ray diffraction (XRD) analysis using a Siemens D501 equipped with Cu K $\alpha$  radiation in a  $\theta/2\theta$  configuration and by transmission electron microscopy (TEM) using a Jeol 3010 operating at 300 keV. Thermogravimetry (TG) and differential scanning calorimetry (DSC) were carried isochronally (10 K/min) under a constant flow of He in a Netzsch Symultaneous Thermal Analyzer STA 409 equipped with a TASC 414/2 controller. Hydrogen sorption kinetics was investigated at 573 K under vacuum or 10 bar hydrogen during desorption and absorption, respectively. The measurements were performed at GKSS using a volumetric Sieverts-type apparatus designed by Hydro Quebec/HERA Hydrogen Storage Systems.

## 3. Results and discussion

Fig. 1 shows the XRD patterns (Cu K $\alpha$ ) for the MgH<sub>2</sub> powders ball milled for 48 h with FeF<sub>3</sub> (pattern a) or NiF<sub>2</sub> (pattern c). In the case of FeF<sub>3</sub>-containing powders, the most intense Bragg peaks that can be observed in the XRD pattern can be identified as coming from the starting materials, i.e. tetragonal MgH<sub>2</sub> (PDF 12-0697) and FeF<sub>3</sub> (PDF 33-0647). Also in the XRD pattern for the NiF<sub>2</sub>-containing powders (pattern b of Fig. 1), the most intense peaks are those of the



Fig. 1. XRD patterns (Cu K $\alpha$ ) for (a) MgH<sub>2</sub> + 5 mol% FeF<sub>3</sub> and (c) MgH<sub>2</sub> + 5 mol% NiF<sub>2</sub> ball milled for 48 h. Results for (b) MgH<sub>2</sub> + 5 mol% FeF<sub>3</sub> and (d) MgH<sub>2</sub> + 5 mol.% NiF<sub>2</sub> after DSC/TG analysis are also shown for comparison.

starting materials, although NiF<sub>2</sub> reflections (PDF 24-0791) are not readily recognized due to an overlapping with MgH<sub>2</sub>. In both patterns, additional reflections from MgO (PDF 45-0946) and  $\gamma$ -MgH<sub>2</sub> (PDF 35-1184) can be observed, as well. The latter is a metastable orthorhombic phase, which has been previously reported to form upon milling of MgH<sub>2</sub> [6]. As for the presence of magnesium oxide, this is likely due to slight oxygen contamination. It is worth noticing that Fe reflections (PDF 6-0696) are detected in the pattern for  $MgH_2 + 5 \text{ mol}\%$ FeF<sub>3</sub>. It can be argued that this could be the result of impurities from milling debris. If that were the case, a comparable amount of iron impurities would be expected to be present also in the NiF<sub>2</sub>-containing powders, the milling conditions being the same for both systems. Yet, no iron peaks can be observed in pattern c of Fig. 1. Thus, the small quantity of iron detected in the as milled  $MgH_2 + 5 \mod 8 FeF_3$  powders likely stems from FeF<sub>3</sub>.

XRD analysis suggests that, besides the formation of limited amounts of  $\gamma$ -MgH<sub>2</sub> and Fe from FeF<sub>3</sub>, the milling process does not induce any clear phase transformation or solid-state reaction. On the other hand, the peak broadening which can be observed in both patterns of Fig. 1 clearly points out that, upon milling, strain and structural defects are introduced into MgH<sub>2</sub>. At the same time, the grain size is significantly reduced and can be estimated to be in the nanometer range. This is confirmed by TEM investigations (not shown), which show that the grain size of MgH<sub>2</sub> ranges from about 100 nm to few tens of nanometers. It should be mentioned that much smaller crystallite sizes, e.g. less than 20 nm, have been reported for MgH<sub>2</sub> milled using milling devices and conditions which are different from those used in this work [7].

Constant-heating DSC and TG analysis were carried out in order to investigate the catalytic effect of FeF<sub>3</sub> and NiF<sub>2</sub> additions on the MgH<sub>2</sub> desorption reaction. In Fig. 2, the DSC traces for as-milled MgH<sub>2</sub> + 5 mol% FeF<sub>3</sub> and MgH<sub>2</sub> + 5 mol% NiF<sub>2</sub> are compared with that for pure MgH<sub>2</sub>



Fig. 2. Constant-heating (10 K/min) DSC trace for  $MgH_2 + 5 \text{ mol}\%$  FeF<sub>3</sub> (solid line),  $MgH_2 + 5 \text{ mol}\%$  NiF<sub>2</sub> (dashed line), and  $MgH_2$  (dotted line) ball milled for 48 h.



Fig. 3. Thermogravimetric analysis for  $MgH_2 + 5 \text{ mol}\%$  FeF<sub>3</sub> (solid line),  $MgH_2 + 5 \text{ mol}\%$  NiF<sub>2</sub> (dashed line), and  $MgH_2$  (dotted line) ball milled for 48 h.

powders ball milled for 48 h under the same experimental conditions-i.e. having the same grain size and with no impurities being detected by XRD. The onset of desorption, which is around 640 K for as-milled MgH<sub>2</sub> powders, decreases significantly for the FeF<sub>3</sub>- and NiF<sub>2</sub>-containing powders. For  $MgH_2 + 5 mol\%$  NiF<sub>2</sub>, desorption starts well below 600 K, whereas, for  $MgH_2 + 5 \mod \%$  FeF<sub>3</sub>, it begins at about 500 K. On the other hand, it should be noticed that, especially for the FeF<sub>3</sub>-containing powders, the desorption reaction is characterized by several endothermic events and appears to occur over a rather broad temperature range. This can be ascribed to the broad distribution of grain sizes which has been observed by TEM for  $MgH_2 + 5 \text{ mol.}\%$  FeF<sub>3</sub>, and which, in turn, results in different activation energies for hydrogen desorption. TG analysis (see Fig. 3) confirms that the endothermic peaks observed in Fig. 2 stem from the hydrogen desorption reaction and are associated to a weight loss of more than 6% for ball-milled MgH<sub>2</sub>, more that 5% for MgH<sub>2</sub> + 5 mol% NiF<sub>2</sub>, and about 4% for MgH<sub>2</sub> + 5 mol% FeF<sub>3</sub>. Such values for the weight loss are lower than what one would expect from the theoretical capacity for MgH<sub>2</sub> (about 7.6 wt.%). This can be explained by taking into account the purity of the starting magnesium hydride powder (90%, the rest being Mg), the slight oxidation of the powders, and the relative content of FeF<sub>3</sub> (18.4 wt.%) or NiF<sub>2</sub> (16.2 wt.%), which all contribute in lowering the total capacity of the systems investigated in this work.

The XRD patterns carried out on  $MgH_2 + 5 \text{ mol}\% \text{ Fe}F_3$ and  $MgH_2 + 5 \text{ mol}\% \text{ Ni}F_2$  powders after the DSC/TG runs are shown in Fig. 1 (patterns b and d, respectively). In both cases, it can be seen that  $MgH_2$  has completely transformed into Mg (PDF 35-0821). At the same time, no peaks from the starting catalysts can be detected, whereas reflections from MgF<sub>2</sub> (PDF 41-1443), Fe (PDF 6-0696) (only in pattern b) and Mg<sub>2</sub>Ni (PDF 35-1225) (only in pattern d) can be observed. This suggests the occurrence, apparently above the desorption temperature, of a displacement reaction between Mg and the catalyst. In one case, Mg reacts with  $FeF_3$  to give  $MgF_2$  and Fe, whereas the reaction between Mg and  $NiF_2$  results in the formation of  $MgF_2$  and  $Mg_2Ni$ .

The formation of a MgF2 surface layer has previously been reported for a Mg<sub>2</sub>Ni alloy, which underwent a F-treatment in aqueous solution [8]. In that case, the authors argued that the formation of such layer, which exhibits a high affinity to hydrogen, is decisive for a rapid initial activation of the alloy. On the other hand, the formation of magnesium fluoride has already been observed directly upon milling of MgH<sub>2</sub> and FeF<sub>3</sub>, in a planetary ball milling device [6,9]. For the systems investigated in this work, magnesium fluoride is not detected by XRD in the as-milled powders. However, its formation at the FeF3/MgH2 or NiF2/MgH2 interfaces, which are created during the repeated fracturing and coldwelding processes occurring upon milling, cannot be ruled out. Indeed, the presence of limited amounts of iron in the as-milled FeF3-containing powders, could be indicative of the mechanically driven solid-state reaction between FeF<sub>3</sub> and MgH<sub>2</sub> to give MgF<sub>2</sub> and Fe. The presence, even in small quantities, of MgF<sub>2</sub> may catalyze the hydrogen desorption, thus explaining the decrease of the desorption temperatures observed for  $MgH_2 + 5 \mod \%$  FeF<sub>3</sub> and  $MgH_2 + 5 \mod \%$ NiF<sub>2</sub>, with respect to ball-milled MgH<sub>2</sub>. As the hydrogen desorption reaction proceeds and more Mg is available, more MgF<sub>2</sub> is formed, further favoring the desorption of hydrogen. Of course, such a picture must be substantiated by more evidences and further investigations are currently being performed to clarify the possible role that MgF<sub>2</sub> might play.

It could also be argued that the decrease of the desorption temperature observed for  $MgH_2 + 5 \mod 8$  FeF<sub>3</sub> is simply due to the Fe, which is formed either upon milling or desorption and which has been reported to exhibit a fairly good catalytic activity [3]. However, when  $MgH_2$  and Fe are milled under the same processing conditions used in this work, the resulting powders do not show the marked decrease of the desorption temperature observed for the  $MgH_2$ –FeF<sub>3</sub> composite powders [9]. Therefore, although it likely contributes significantly to the overall sorption behavior, Fe cannot be, in our case, the sole responsible for the improved desorption.

Finally, preliminary investigations on the H-sorption kinetics have been carried out to further estimate the catalytic activity of the fluoride additions and to test the effect of cycling. Fig. 4 shows the two consecutive runs for desorption (at 573 K under vacuum) and absorption (at 573 K under 10 bar hydrogen) as measured for the as-milled  $MgH_2$  + 5 mol% FeF<sub>3</sub> system. It can be seen that, during the first desorption run, 4 wt.% of hydrogen is desorbed already after 600 s, whereas the same amount is desorbed after less than 500 s during the second run. As for the absorption, for both runs, it is complete after about 1200 s, the hydrogen uptake being slightly faster during the second run. This clearly indicates that, at least after one cycle, the H-sorption behavior not only is preserved, but it actually improves. A much faster kinetics have previously been reported for  $MgH_2 + 5$  at.% V [10] and for  $MgH_2 + 0.5 \text{ mol}\% \text{ Nb}_2O_5$  [4]. Nonetheless, our



Fig. 4. Sorption kinetics for as-milled  $MgH_2 + 5 \mod \% FeF_3$ at 573 K. Desorption was carried out under vacuum, whereas absorption was performed under 10 bar hydrogen.

results can be regarded as very promising, if one considers that the grain size for the as milled powders is not homogeneous, as mentioned above few grains being larger that 100 nm. A significant improvement in the sorption kinetics should be expected if the milling parameters are adjusted and homogeneous grain sizes, in the order of about 20 nm, are achieved.

## 4. Conclusions

Ball milling techniques were used to produce  $MgH_2$ nanocomposites containing FeF<sub>3</sub> and NiF<sub>2</sub>. It was shown that fluoride additions are beneficial, with respect to the Hsorption behavior. In the case of FeF<sub>3</sub> additions, the desorption temperature, as measured by isochronal DSC (10 K/min), is as low as 500 K and the time necessary for H-desorption after one cycle at 573 K is less than 500 s. Further investigation are required to clarify the catalytic role played by  $MgF_2$ , the latter being formed during desorption.

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